



PERFORMANCE CURVE

MODEL XS-3 3" x 3"

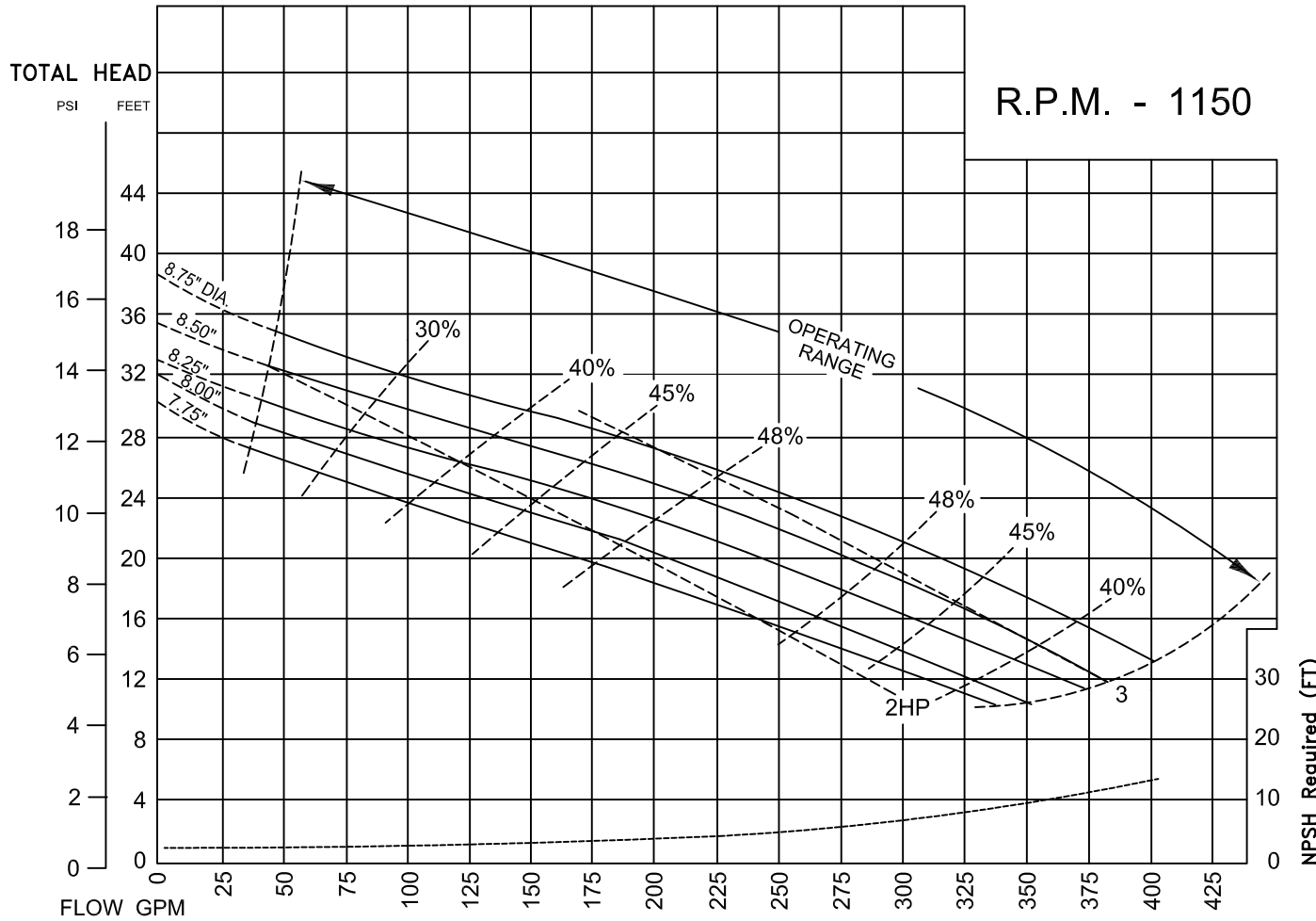
DATA

Impeller dia. - 7<sup>3</sup>/<sub>4</sub>" to 8<sup>3</sup>/<sub>4</sub>"

R.P.M. - 1150

Solids, max. dia. - 2<sup>1</sup>/<sub>2</sub>"

NOT TO SCALE



PRIMING LIFT

| Dia.:                           | Feet: |
|---------------------------------|-------|
| 7 <sup>3</sup> / <sub>4</sub> " | 8-ft  |
| 8"                              | 8-ft  |
| 8 <sup>1</sup> / <sub>4</sub> " | 9-ft  |
| 8 <sup>1</sup> / <sub>2</sub> " | 12-ft |
| 8 <sup>3</sup> / <sub>4</sub> " | 16-ft |

Before using this table verify application NPSH

When pump is operating, the **SUCTION LIFT** is limited by the available **NPSH** which is the corrected atmospheric pressure minus the dynamic suction lift, vapor pressure loss and 2-foot safety factor. This net available **NPSH** must exceed the required **NPSH** of the pump or a reduction of capacity, loss of efficiency, noise, vibration and cavitation will result. Calculate the dynamic suction lift from the low liquid level to the centerline of the impeller. When pump is priming, it is limited by the dry **PRIMING LIFT** which is the vertical distance from the high liquid level to the centerline of the impeller.

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